

## **Opportunities and Limits of CO<sub>2</sub> Recycling in a Circular Carbon Economy**

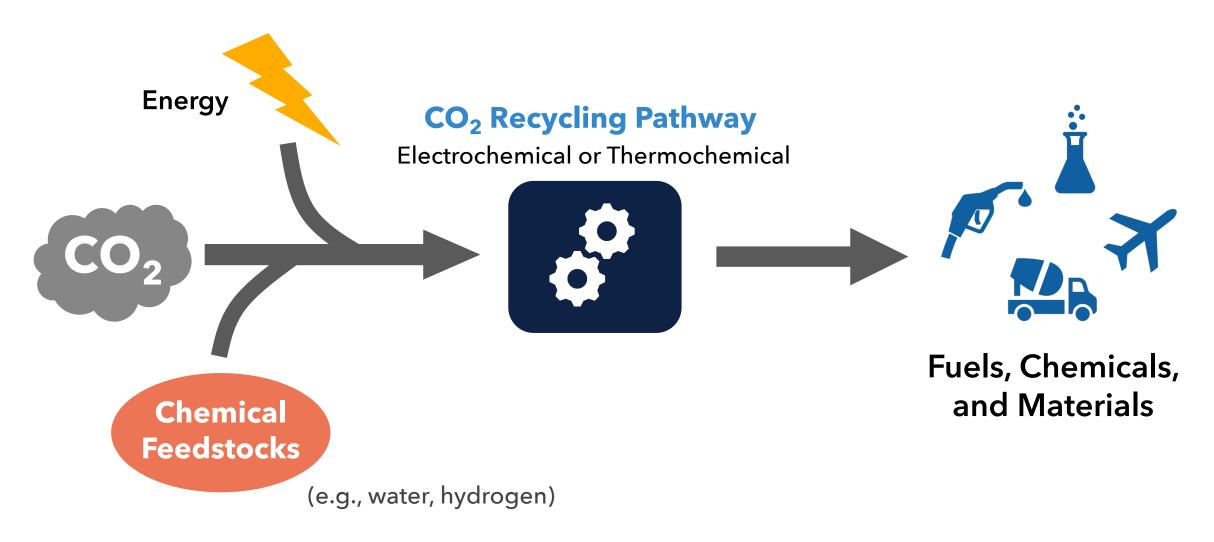


### The need for CO<sub>2</sub> recycling

- We rely on many products that are carbon-intensive to produce but have limited alternatives
  - Aviation fuels, concrete, plastics, etc.
- 30% of global CO<sub>2</sub> emissions are in 'hard to abate' sectors



## CO<sub>2</sub> recycling – converting CO<sub>2</sub> into valuable products



### An unrealized opportunity...so far

- Chemical processes that consume CO<sub>2</sub> instead of generating it
- Reduces emissions of production
- Products have economic value in existing markets
- CO<sub>2</sub> recycling has remained difficult to deploy
- Need well-informed policy support



We modeled 19  $CO_2$  recycling pathways to provide a better understanding of the current state of  $CO_2$  recycling, opportunities, and challenges to reach global scale.



## Sections of Analysis

- 1. Estimated Cost of Production and Cost Sensitivities
- 2. Life-Cycle Carbon Abatement Potential
- **3. Effective Carbon Price**
- **4. Critical Infrastructure Needs**
- **5. Policy Recommendations**

### **Eight electrochemical pathways**

Product	Process	Feedstocks
Hydrogen	Water electrolysis	H <sub>2</sub> O
Carbon monoxide (CO)	Electrochemical CO <sub>2</sub> reduction	CO <sub>2</sub> , H <sub>2</sub> O
Methane		
Methanol		
Ethylene		
Ethane		
Ethanol		
Syngas		

### **Eleven thermochemical pathways**

Product	Process	Feedstocks
Light olefins incl. ethylene	CO <sub>2</sub> hydrogenation	CO <sub>2</sub> , H <sub>2</sub>
	Fischer-Tropsch (F-T) synthesis	CO, H <sub>2</sub>
Methane	Sabatier process	CO <sub>2</sub> , H <sub>2</sub>
Methanol	CO <sub>2</sub> hydrogenation	CO <sub>2</sub> , H <sub>2</sub>
Ethanol	Lignocellulosic biomass fermentation	Lignocellulosic biomass
Syngas	Reverse water-gas shift (RWGS) reaction	CO <sub>2</sub> , H <sub>2</sub>
Jet fuel	CO <sub>2</sub> hydrogenation	CO <sub>2</sub> , H <sub>2</sub>
	Fischer-Tropsch synthesis	CO, H <sub>2</sub>
Urea	Bosch-Meiser process	CO <sub>2</sub> , NH <sub>3</sub>
Precast concrete	Concrete carbonation curing	CO <sub>2</sub> , concrete
All concretes	CarbonCure process	CO <sub>2</sub> , concrete

## Analysis design

- Pathways consume low-carbon inputs
  - Renewable electricity and chemical feedstocks that are made electrochemically with renewable power
- Pathways scaled to supply current global demand for their product
- Globally representative cost estimates
- Market parity: cost of production equals selling price

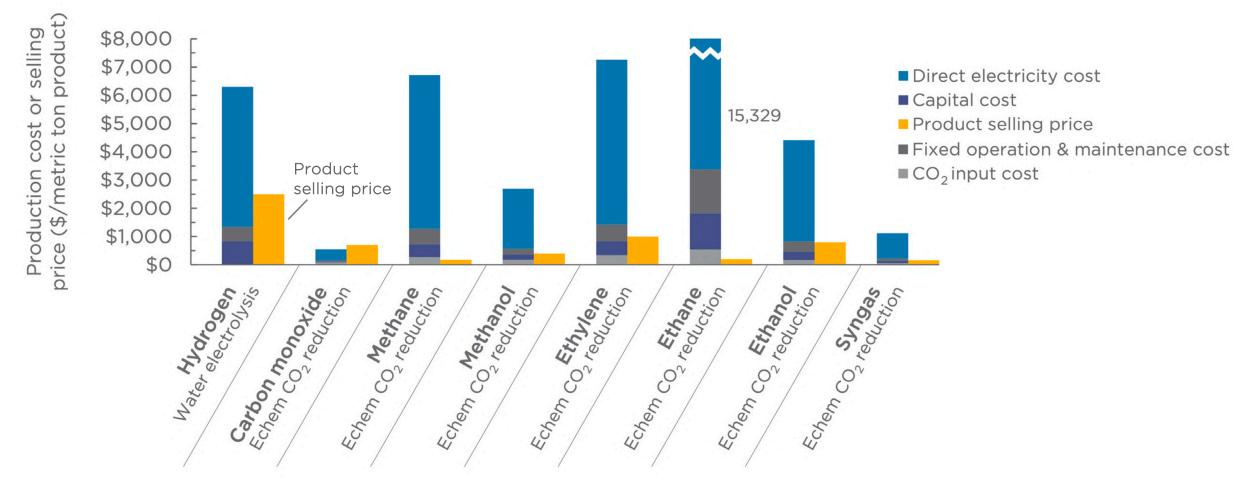
## **Key numerical assumptions**

Parameter	Value
Renewable electricity price	\$0.095/kWh
Green hydrogen feedstock price	\$6.3/kg H <sub>2</sub>
CO <sub>2</sub> feedstock price	\$50/tCO <sub>2</sub>
Electrolyzer capital cost	\$1,000/kW

- Electricity price is globally representative and includes non-generation costs
- CO<sub>2</sub> feedstock is from point-source carbon capture
- Input prices may fall significantly over time and lower costs are available today in limited contexts

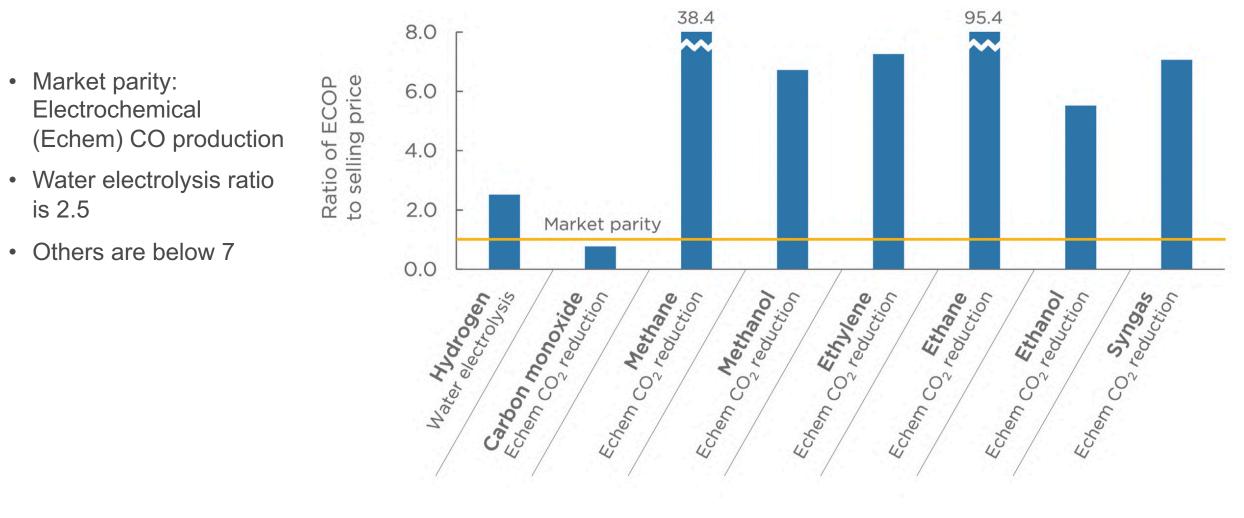
## **1. Estimated Cost of Production (ECOP)**

## Costs of electrochemical pathways are high, and dominated by electricity costs

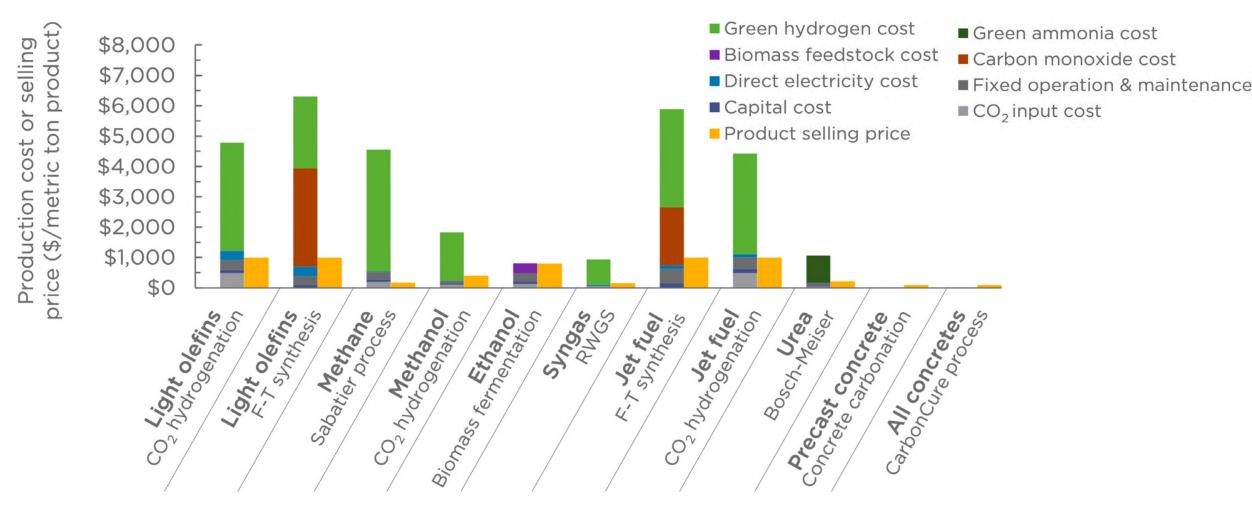


• But capital cost and fixed operation & maintenance alone are greater than selling price for many pathways

## Ratio of ECOP to selling price for electrochemical pathways demonstrates distance from market parity



## Costs of thermochemical pathways are slightly lower, and main component is green hydrogen feedstock cost

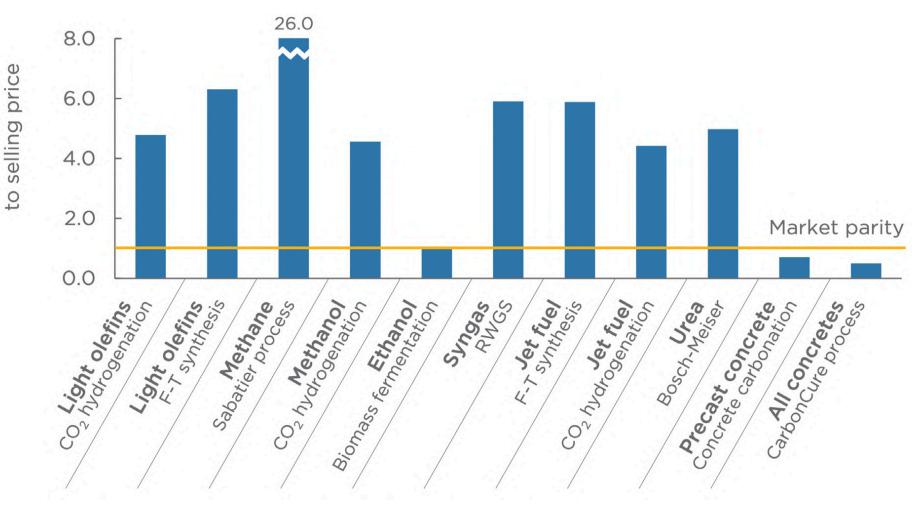


• Non-hydrogen costs exceed selling price for many pathways

## Ratio of ECOP to selling price for thermochemical pathways is lower, but far exceeds market parity

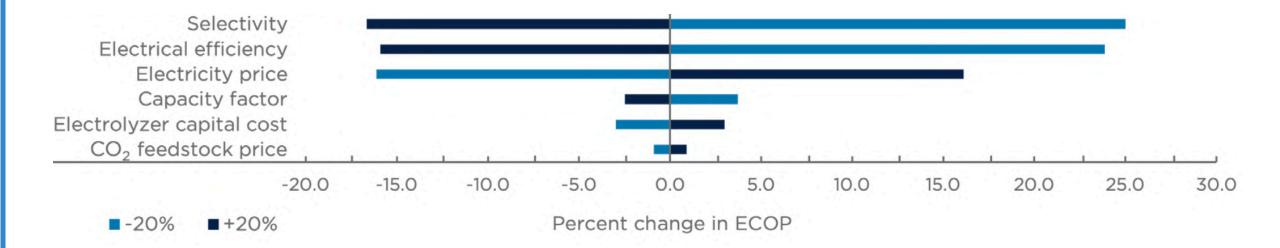
 Market parity: Ethanol from lignocellulosic biomass and the concrete production pathways Ratio of ECOP

 Others have ratio below 6



### Sensitivity analysis shows key cost drivers

#### Percent change in ECOP as a result of a 20% change in an input value



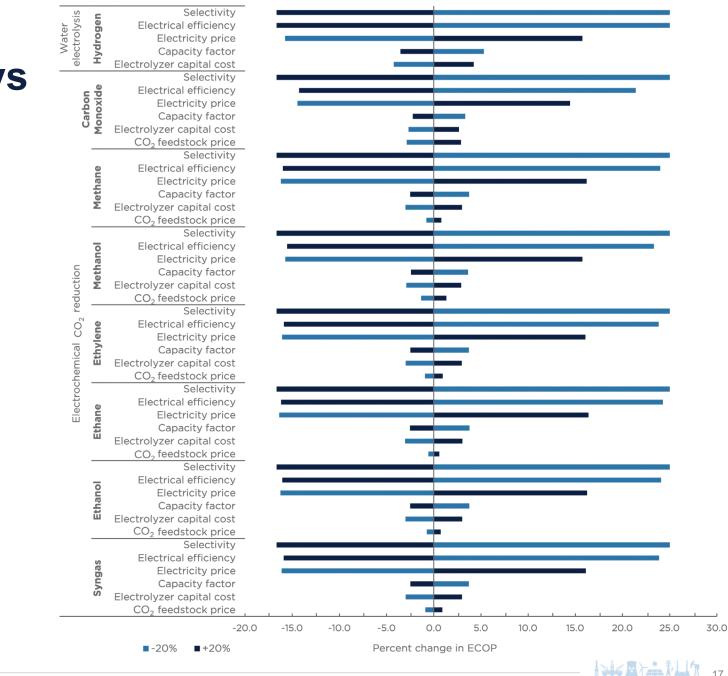
### **Electrochemical pathways**

#### Key cost drivers:

- **Selectivity** (ability to avoid unwanted side reactions)
- Electrical energy efficiency
- Electricity price
  - Slower to improve

#### Weaker cost drivers:

- Capacity factor
- Electrolyzer capital cost
- CO<sub>2</sub> feedstock price
  - DAC would have small effect on ECOP



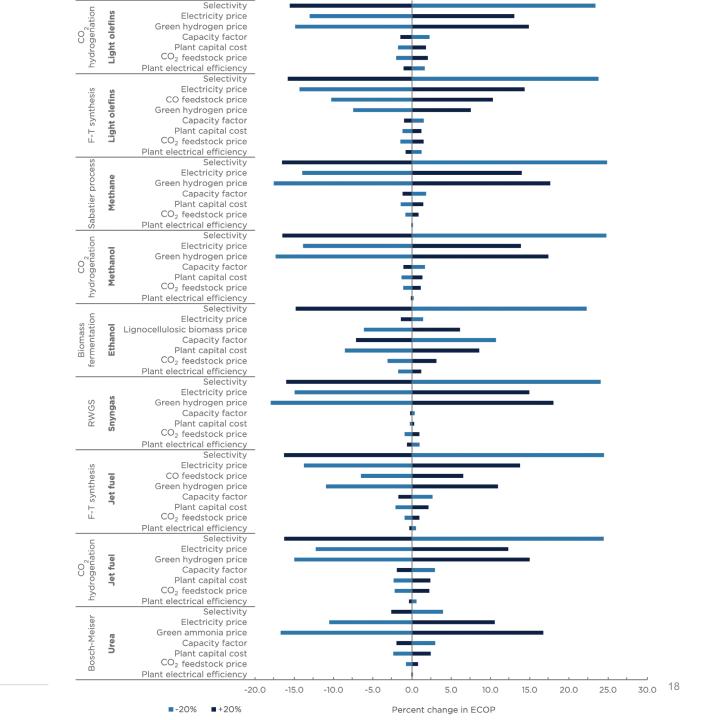
### **Thermochemical pathways**

#### Key cost drivers:

- Selectivity
- Electricity price
- Hydrogen price

#### Weaker cost drivers:

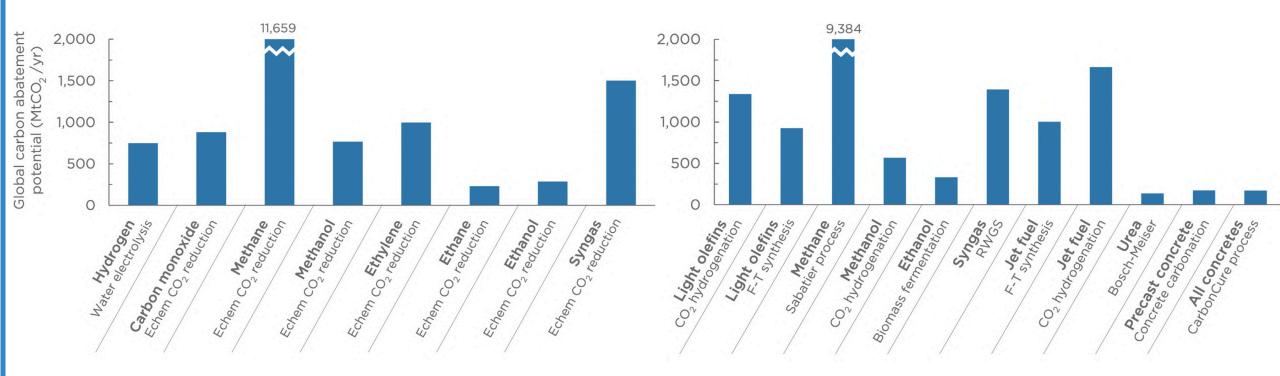
- Capacity factor
- Capital cost
- CO<sub>2</sub> feedstock price



## 2. Life-Cycle Carbon Abatement Potential

# Pathways have a combined carbon abatement potential of 6.8 GtCO<sub>2</sub>/yr

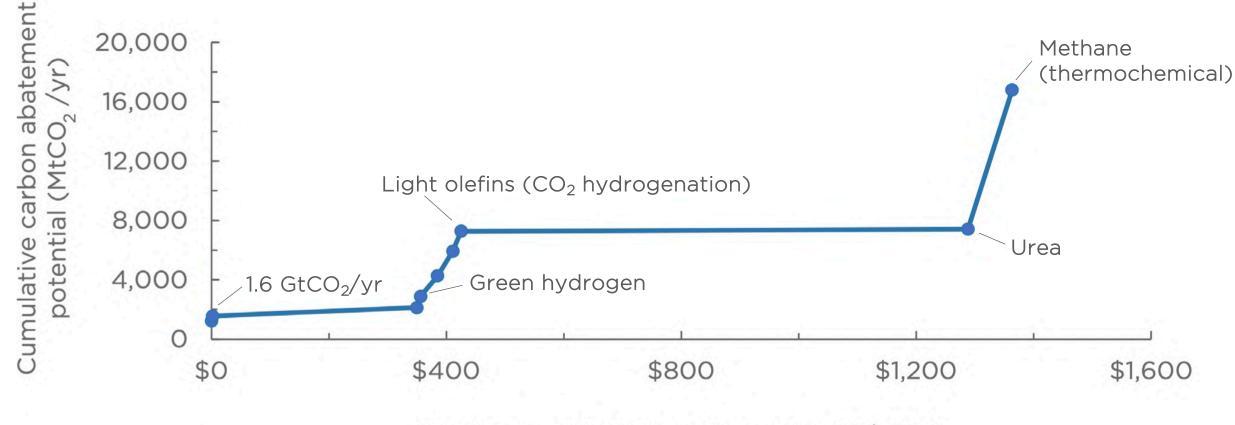
#### **Contingent on use of low-carbon electricity and feedstocks**



Carbon abatement is emissions reduction of displacing conventional production with CO<sub>2</sub> recycling

## 3. Effective Carbon Price and Gross Subsidies

## Cumulative abatement potential available at market parity as a function of effective carbon price



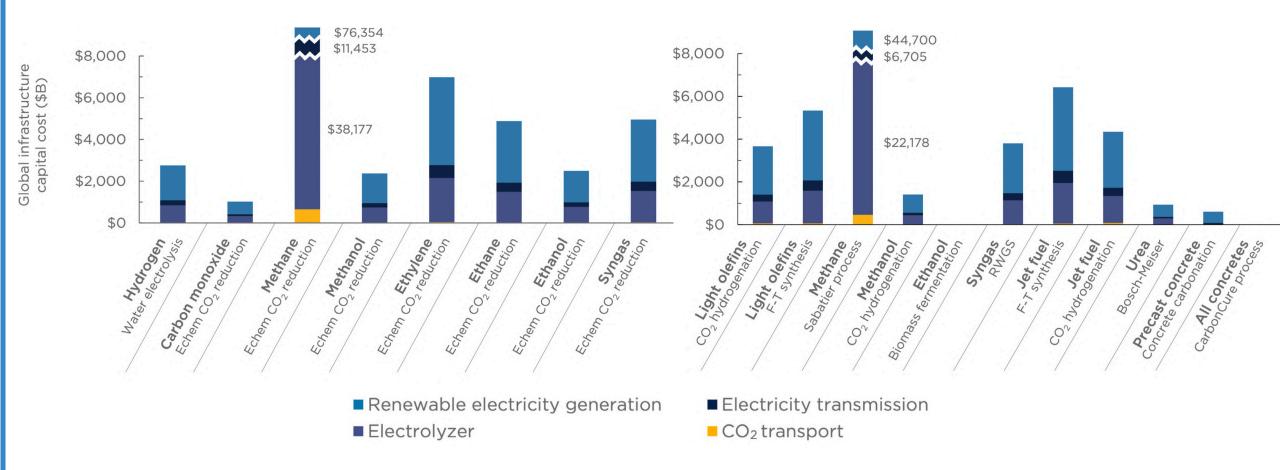
Breakeven effective carbon price  $(\frac{1}{tCO_2})$ 

## **4. Critical Infrastructure Needs**

## Pathways have massive global consumption of electricity and feedstocks

- Pathways consume a combined **36,700 TWh/yr** of low-carbon electricity at global scale
  - Current global electricity consumption: ~26,000 TWh/yr
- Most thermochemical pathways consume ~80 MtH<sub>2</sub>/yr each as feedstock low-carbon hydrogen
  - IEA NZE in 2030: 140 MtH<sub>2</sub>/yr global low-carbon hydrogen supply
- Pathways consume a combined **5.3 GtCO<sub>2</sub>/yr** as feedstock CO<sub>2</sub>
  - Currently ~0.2 GtCO<sub>2</sub>/yr consumed globally in CO<sub>2</sub> recycling

## Trillions of dollars of capital investment in global critical infrastructure needed



- Majority renewable electricity capacity (8,400 GW total)
- CO<sub>2</sub> transport capital costs comparatively negligible

## **Key findings**

- Costs of CO<sub>2</sub> recycling are high and dominated by input costs (electricity and feedstocks)
- Pathways can be classified by ratio of ECOP to selling price
- Main cost drivers are catalyst selectivity, catalyst energy efficiency, and prices of inputs
- Pathways have a combined carbon abatement potential of 6.8 GtCO<sub>2</sub>/yr
- High effective carbon price consistent with market parity
- Trillions of dollars of critical infrastructure needed per pathway, mainly renewables and electrolyzers

## **5. Policy Recommendations**

## **Ensure CO<sub>2</sub> recycling pathways consume low-carbon inputs**

High carbon abatement can only be achieved using low-carbon electricity and low-carbon H<sub>2</sub>, syngas, and/or ammonia feedstocks.

Can use CO<sub>2</sub> from direct air capture or biomass

### **Prioritize pathways strategically**

#### For market scale: (market parity)

- Electrochemical CO production
- Ethanol from lignocellulosic biomass
- Precast concrete carbonation curing
- CarbonCure concrete process

#### For early market entry: (ECOP to selling price ratio < 5)

- Green hydrogen
- CO<sub>2</sub> hydrogenation to light olefins, methanol, and jet fuel
- CO<sub>2</sub> recycling urea production

#### For further technological innovation: (ratio < 8)

 All pathways (incl. Echem CO<sub>2</sub> reduction, F-T synthesis, RWGS)

#### **Deprioritize:** (ratio > 25)

- Electrochemical methane and ethane production
- Sabatier process methane production

## Use RD&D agenda focused on catalyst innovation to bring down costs

Improving the activity and selectivity of catalysts will reduce electricity/feedstock costs and alleviate demand on critical infrastructure.

**Catalyst performance is an efficiency lever** 

## **Create demand pull for early market CO<sub>2</sub> recycling products**

Demand pull policies can create early markets for CO<sub>2</sub> recycling and help achieve scale.

Public procurement, financial incentives, milestone payments

### **Promote buildout of critical infrastructure**

Accelerated buildout of low-carbon electricity, transmission, electrolyzers, and CO<sub>2</sub> transport infrastructure is needed to enable CO<sub>2</sub> recycling at scale.

Remove barriers to infrastructure projects and provide/enable investment

## Our findings can provide granularity for American Jobs Plan

Initial plan included \$35 billion in climate innovation and public procurement of cleaner cement.

 Use findings to guide CO<sub>2</sub> recycling innovation funding and define public procurement standards

## Include demonstration of market-ready CO<sub>2</sub> recycling pathways in American Jobs Plan

Initial plan included \$15 billion in climate demonstration (CO<sub>2</sub> recycling not listed) + 15 low-carbon hydrogen demonstration and 10 carbon capture retrofits

#### Include the following CO<sub>2</sub> recycling pathways:

- Electrochemical CO production
- CO<sub>2</sub> hydrogenation to light olefins, methanol, and jet fuel
- CO<sub>2</sub> recycling urea production

## Thank You

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### Technical inputs and assumptions

Process	Product	Global demand (Mt product/yr)	Gravimetric energy density (kWh/kg)	Echem electrical energy efficiency	Thermochem plant electrical energy efficiency	Hydrogen selectivity	Carbon selectivity	Faradaic efficiency	Conversion	References
Electrochemical pa	thways									
Water electrolysis	Hydrogen	70	39.4	0.75			0	1.0	1.0	[10],[20],[49]
Electrochemical CO <sub>2</sub> reduction	Carbon monoxide	320	2.3	0.55	7	7	1.0	1.0	1.0	[60-63]
Electrochemical CO <sub>2</sub> reduction	Methane	2,920	15.2	0.53		$\overline{a}_{2}$	0.57	0.56	0.90	[64-66]
Electrochemical CO <sub>2</sub> reduction	Methanol	140	6.4	0.54			0.42	0.59	0.90	[44],[67-70]
Electrochemical $CO_2$ reduction	Ethylene	150	13.9	0.48	-		0.51	0.52	0.90	[43],[71-73]
Electrochemical CO <sub>2</sub> reduction	Ethane	40	14.4	0.41			0.30	0.24	0.90	[74-75]
Electrochemical CO <sub>2</sub> reduction	Ethanol	87	8.3	0.45			0.65	0.54	0.90	[76-78]
Electrochemical CO <sub>2</sub> reduction	Syngas	691	3.9	0.51			0.72	0.76	1.0	[79-80]
Thermochemical pa	thways									
CO <sub>2</sub> hydrogenation	Light olefins incl. ethylene	150	13.9		0.75	0.68	0.36		0.90	[81-85]
F-T synthesis	Light olefins incl. ethylene	150	13.9		0.75	0.64	0.34		0.90	[86-91]
Sabatier process	Methane	2,920	15.2		0.75	0.79	0.72		1.0	[92-94]
CO <sub>2</sub> hydrogenation	Methanol	140	6.4		0.75	0.75	0.75		0.90	[44],[95-96]
Biomass fermentation	Ethanol	87	8.3		0.75		1.0		0.76	[97-98]
RWGS	Syngas	691	3.9		0.75	1	0.90		1.0	[99-100]
F-T synthesis	Jet fuel	200	11.9		0.75	0.58	0.56		0.90	[50],[101-104]
CO <sub>2</sub> hydrogenation	Jet fuel	200	11.9		0.75	0.56	0.35		0.90	[19],[83], [105-107]
Bosch-Meiser	Urea	208	2.9		0.75	0.72	1.0		0.88	[108-109]
Concrete carbonation	Precast concrete	5,974			0.75					[110-112]
CarbonCure process	All concretes	33,000			0.75					[113]

# Plant assumptions

Process	ocess Product		Electrolyzer capital cost (\$/kW)	Plant capital cost (\$/ton/ yr-capacity)	Equipment lifetime (yr)	
Electrochemical pathw	/ays					
Water electrolysis	Hydrogen	0.5	1,000		15	
Electrochemical CO <sub>2</sub> reduction	Carbon monoxide	0.5	1,000	1	30	
Electrochemical CO <sub>2</sub> reduction	Methane	0.5	1,000		30	
Electrochemical CO <sub>2</sub> reduction	Methanol	0.5	1,000		30	
Electrochemical CO <sub>2</sub> reduction	Ethylene	0.5	1,000		30	
Electrochemical CO <sub>2</sub> reduction	Ethane	0.5	1,000		30	
Electrochemical CO <sub>2</sub> reduction	Ethanol	0.5	1,000		30	
Electrochemical CO <sub>2</sub> reduction	Syngas	0.5	1,000	7	30	
Thermochemical path	ways					
CO <sub>2</sub> hydrogenation	Light olefins incl. ethylene	0.9	-	2,741	30	
F-T synthesis	Light olefins incl. ethylene	0.9		2,447	30	
Sabatier process	Methane	0.9		2,111	30	
CO <sub>2</sub> hydrogenation	Methanol	0.9		777	30	
Biomass fermentation	Ethanol	0.9	1	2,226	30	
RWGS	Syngas	0.9		84	30	
F-T synthesis	Jet fuel	0.9	/	3,969	30	
CO <sub>2</sub> hydrogenation	Jet fuel	0.9		3,320	30	
Bosch-Meiser	Urea	0.9		819	30	
Concrete carbonation	Precast concrete	0.9			30	
CarbonCure process	All concretes	0.9			30	

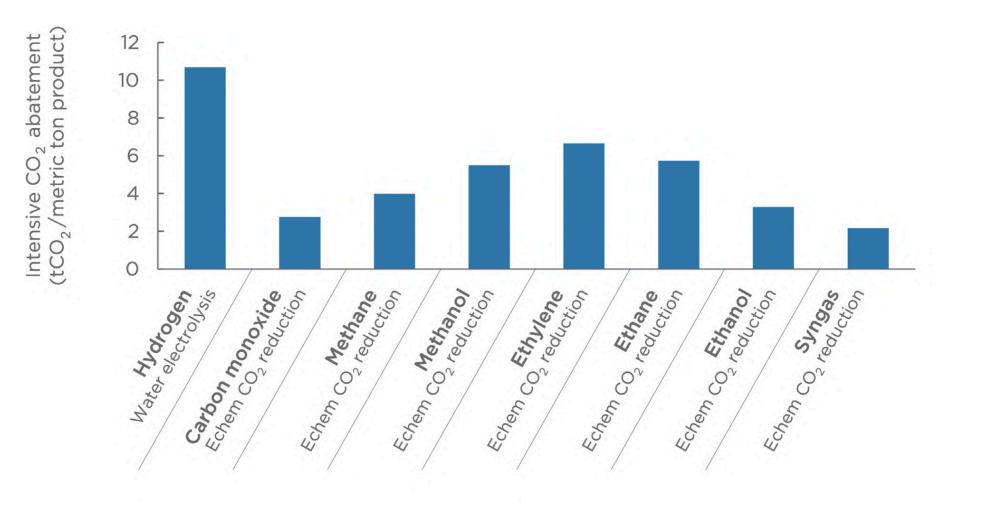
# Financial assumptions

Parameter	Value
Renewable electricity price (\$/kWh)	0.095
Green hydrogen feedstock price (\$/tH <sub>2</sub> )	6,302
CO <sub>2</sub> feedstock price (\$/tCO <sub>2</sub> ) <sup>16</sup>	50
CO feedstock price (\$/tCO)	546
Green ammonia feedstock price (\$/tNH₃)	1,573
Lignocellulosic biomass feedstock price (\$/dry ton)	65
CO <sub>2</sub> transport pipeline network capital cost (\$/tCO <sub>2</sub> /yr capacity) <sup>15</sup>	42
Transmission capital cost (\$/kW renewable generation capacity) <sup>51</sup>	300
Renewable electricity carbon intensity (gCO <sub>2</sub> /kWh) <sup>21</sup>	25
Weighted average cost of capital (WACC)	5%
Fixed O&M percentage of capex electrolyzer	4%
Fixed O&M percentage of capex thermochemical plant	10%
Capacity factor of renewable mix used to determine GW capacity needs	50%

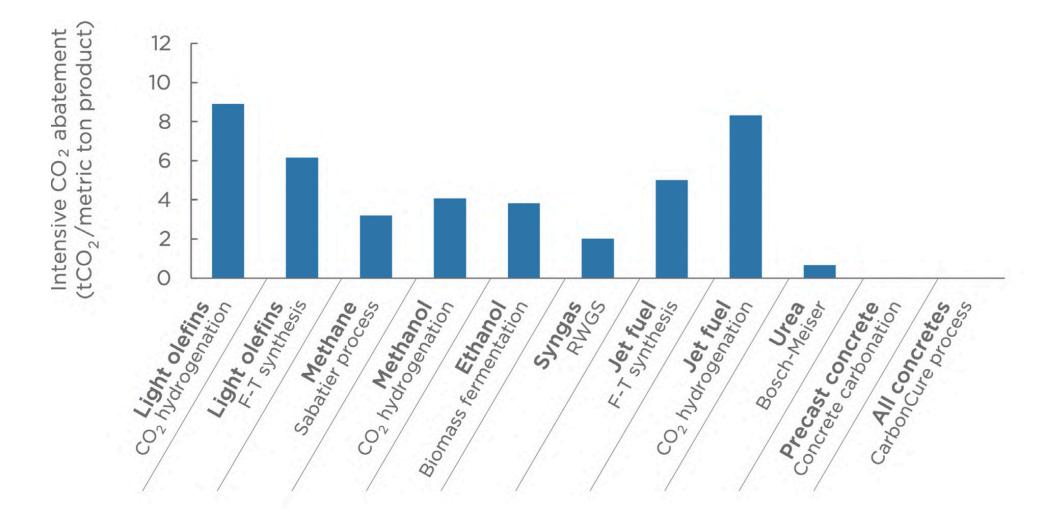
# Results summary

Product	Process	Product selling price (\$/metric ton)	Estimated cost of production (\$/metric ton product)	ECOP/selling price ratio	Carbon abatement potential (MtCO <sub>2</sub> /yr)	Intensive CO <sub>2</sub> abatement (tCO <sub>2</sub> /metric ton product)	Marginal abatement cost (\$/tCO <sub>2</sub> )	Critical infrastructure capital cost (\$B)
Electrochemi	cal pathways							
Hydrogen	Water electrolysis	2,500	6,302	2.5	749	10.7	589	2,757
Carbon monoxide	Electrochemical CO <sub>2</sub> reduction	700	546	0.8	882	2.8	198	1,023
Methane	Electrochemical CO <sub>2</sub> reduction	175	6,714	38.4	11,659	4.0	1,681	126,635
Methanol	Electrochemical CO <sub>2</sub> reduction	400	2,689	6.7	768	5.5	490	2,372
Ethylene	Electrochemical CO <sub>2</sub> reduction	1,000	7,258	7.3	997	6.7	1,091	6,984
Ethane	Electrochemical CO <sub>2</sub> reduction	196	18,705	95.4	230	5.7	3,260	4,881
Ethanol	Electrochemical CO <sub>2</sub> reduction	800	4,416	5.5	286	3.3	1,341	2,488
Syngas	Electrochemical CO <sub>2</sub> reduction	158	1,116	7.1	1,501	2.2	491	4,961
Thermochemi	ical pathways							
Light olefins incl. ethylene	CO <sub>2</sub> hydrogenation	1,000	4,789	4.8	1,337	8.9	537	3,661
Light olefins incl. ethylene	F-T synthesis	1,000	6,311	6.3	925	6.2	1,024	5,337
Methane	Sabatier process	175	4,555	26.0	9,384	3.2	1,417	74,048
Methanol	CO <sub>2</sub> hydrogenation	400	1,824	4.6	570	4.1	448	1,411
Ethanol	Biomass fermentation	800	809	1.0	333	3.8	211	0
Syngas	RWGS	158	934	5.9	1,393	2.0	464	3,797
Jet fuel	F-T synthesis	1,000	5,885	5.9	1,003	5.0	1,174	6,417
Jet fuel	CO <sub>2</sub> hydrogenation	1,000	4,423	4.4	1,664	8.3	532	4,339
Urea	Bosch-Meiser	215	1,071	5.0	138	0.7	1,611	936
Precast concrete	Concrete carbonation	100	70	0.7	174	0.03	672	612
All concretes	CarbonCure process	100	49	0.5	170	0.01	-156	0

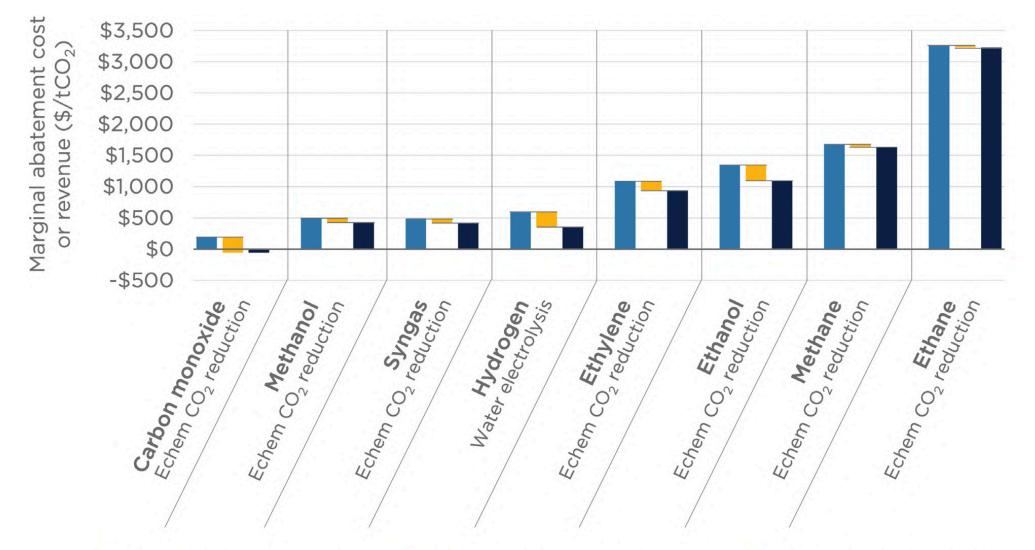
#### Intensive CO<sub>2</sub> abatement of electrochemical pathways



#### **Intensive CO<sub>2</sub> abatement of thermochemical pathways**

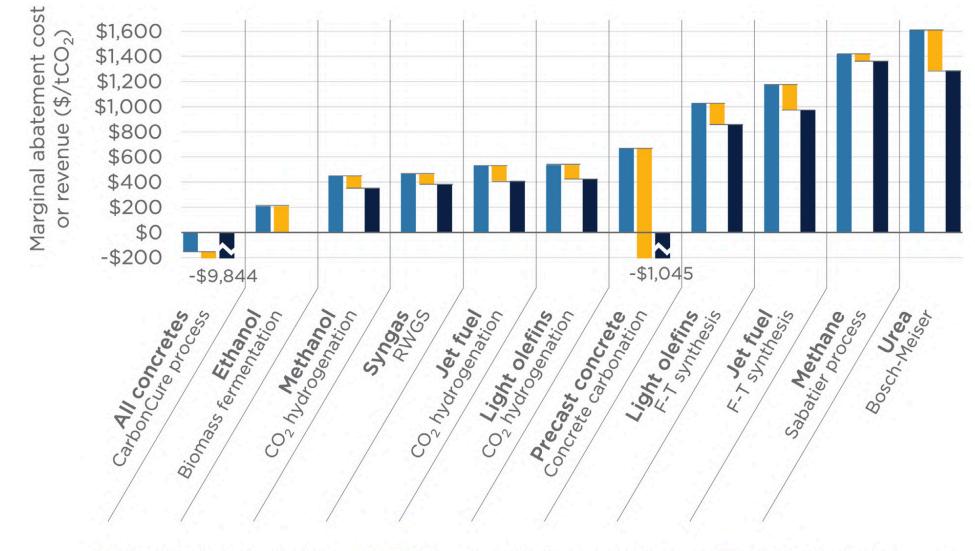


### Marginal abatement cost and revenues for electrochemical pathways



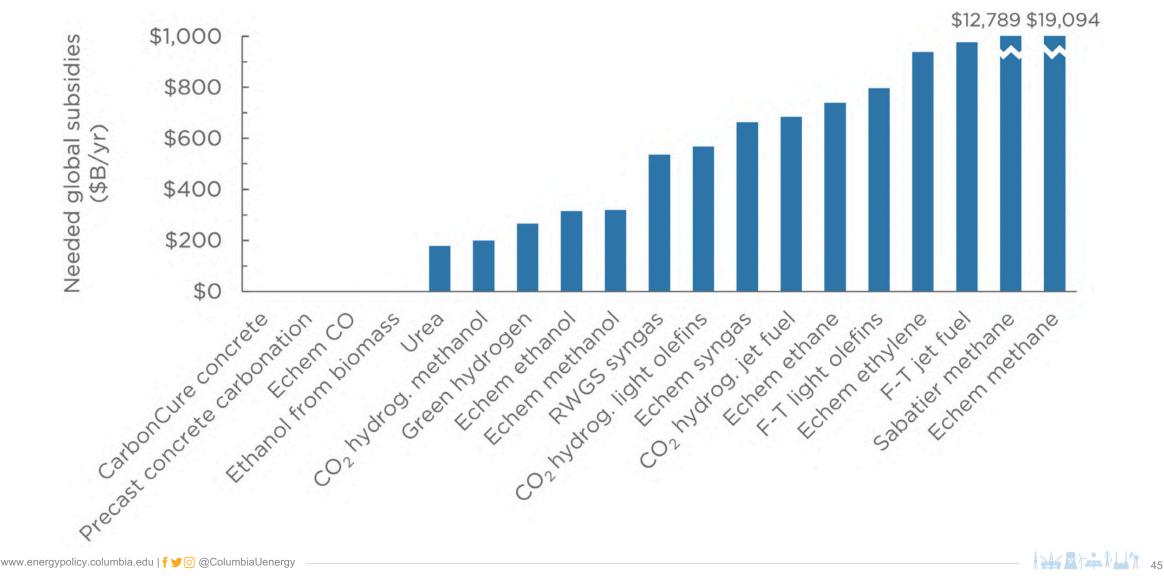
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### Marginal abatement cost and revenues for thermochemical pathways

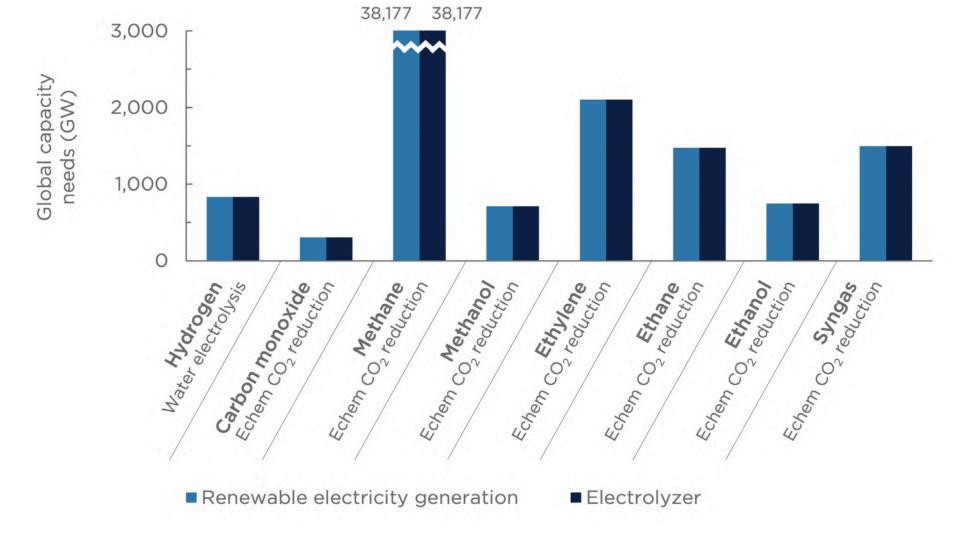


Marginal abatement cost 📕 Marginal abatement revenue 📕 MAC after revenues

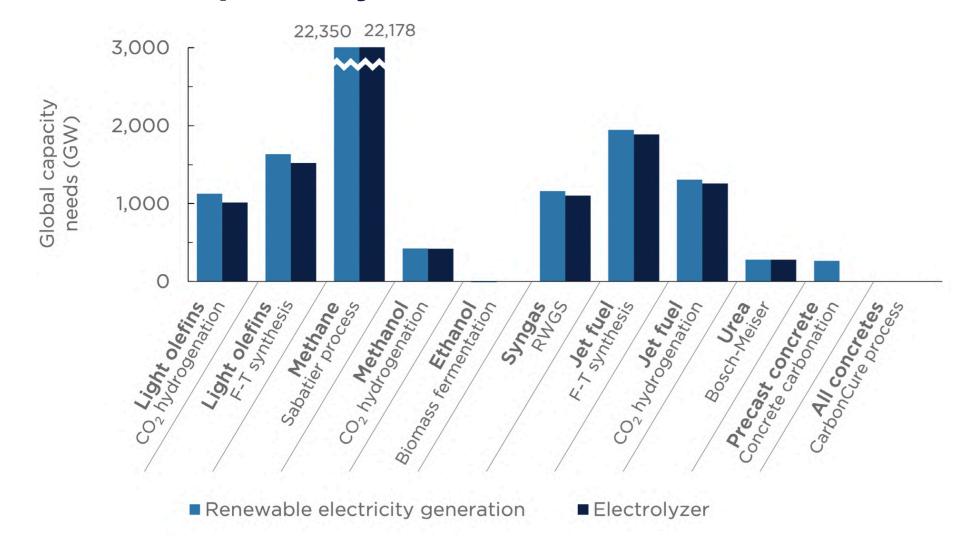
## Hundreds of billions of dollars in gross global subsidies needed to close cost-price gap



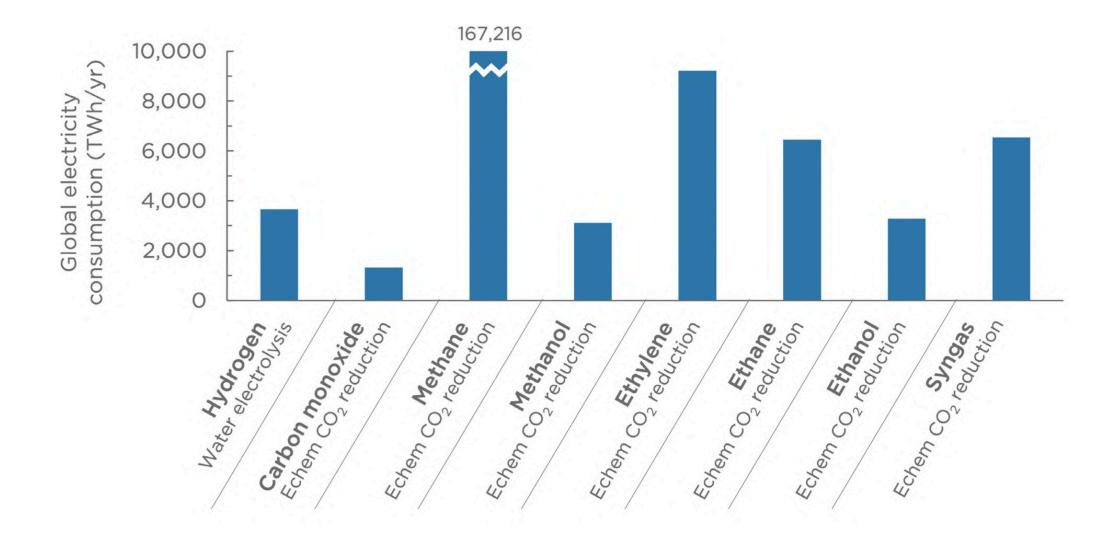
## Global renewables and electrolyzer capacity for electrochemical pathways



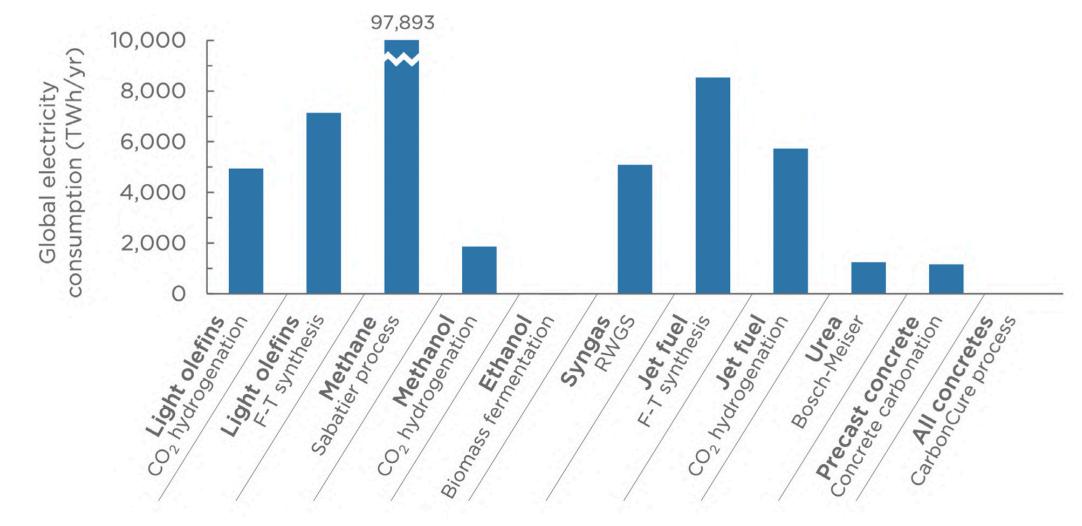
## Global renewables and electrolyzer capacity for thermochemical pathways



### **Global electricity consumption of electrochemical pathways**



### **Global electricity consumption of thermochemical pathways**



### **Global hydrogen consumption of thermochemical pathways**

